



AACHENER VERFAHRENSTECHNIK

General Considerations for Process Modelling on a Thermochemical Basis

GTT-Workshop 4. - 6.6.2008

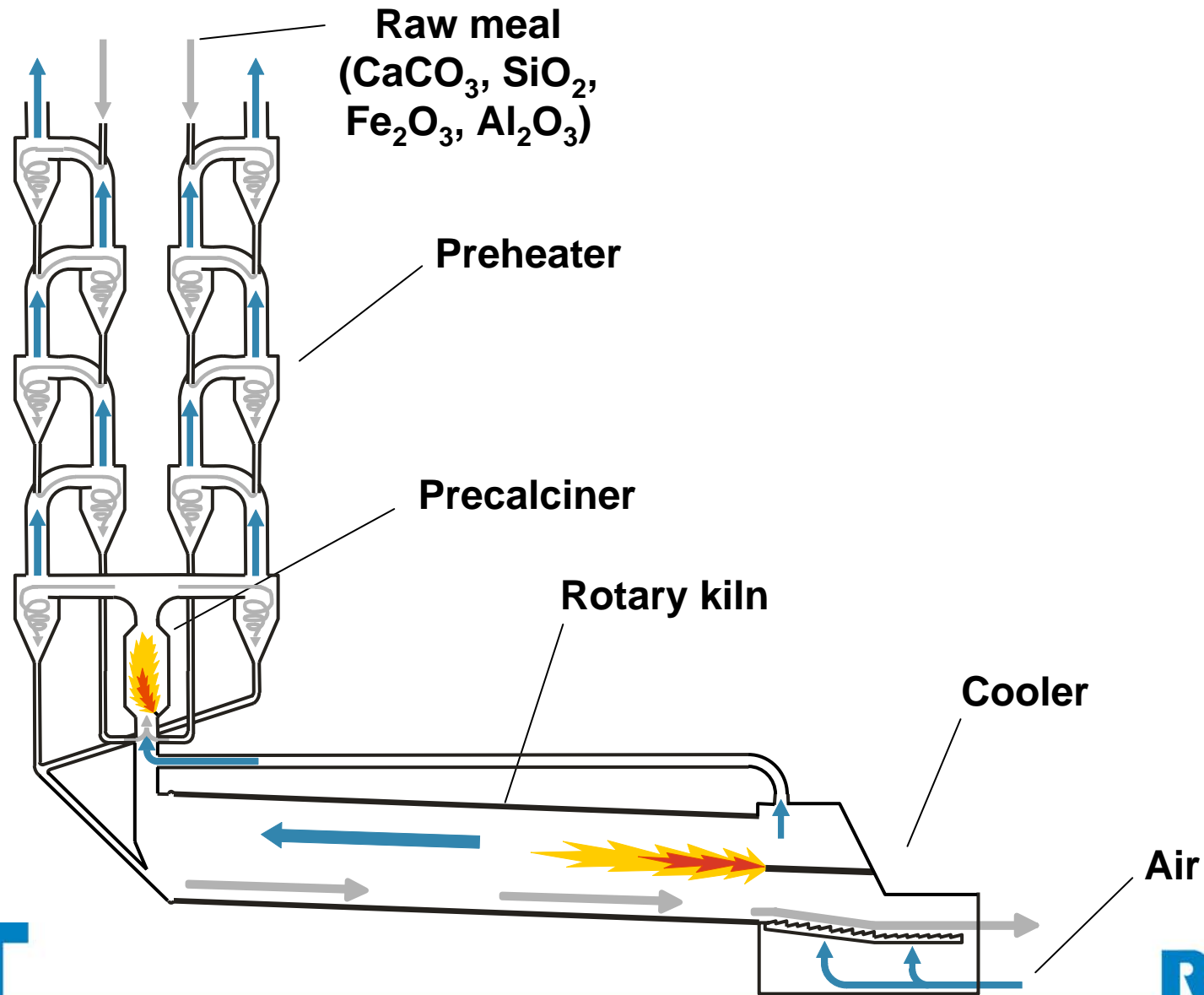
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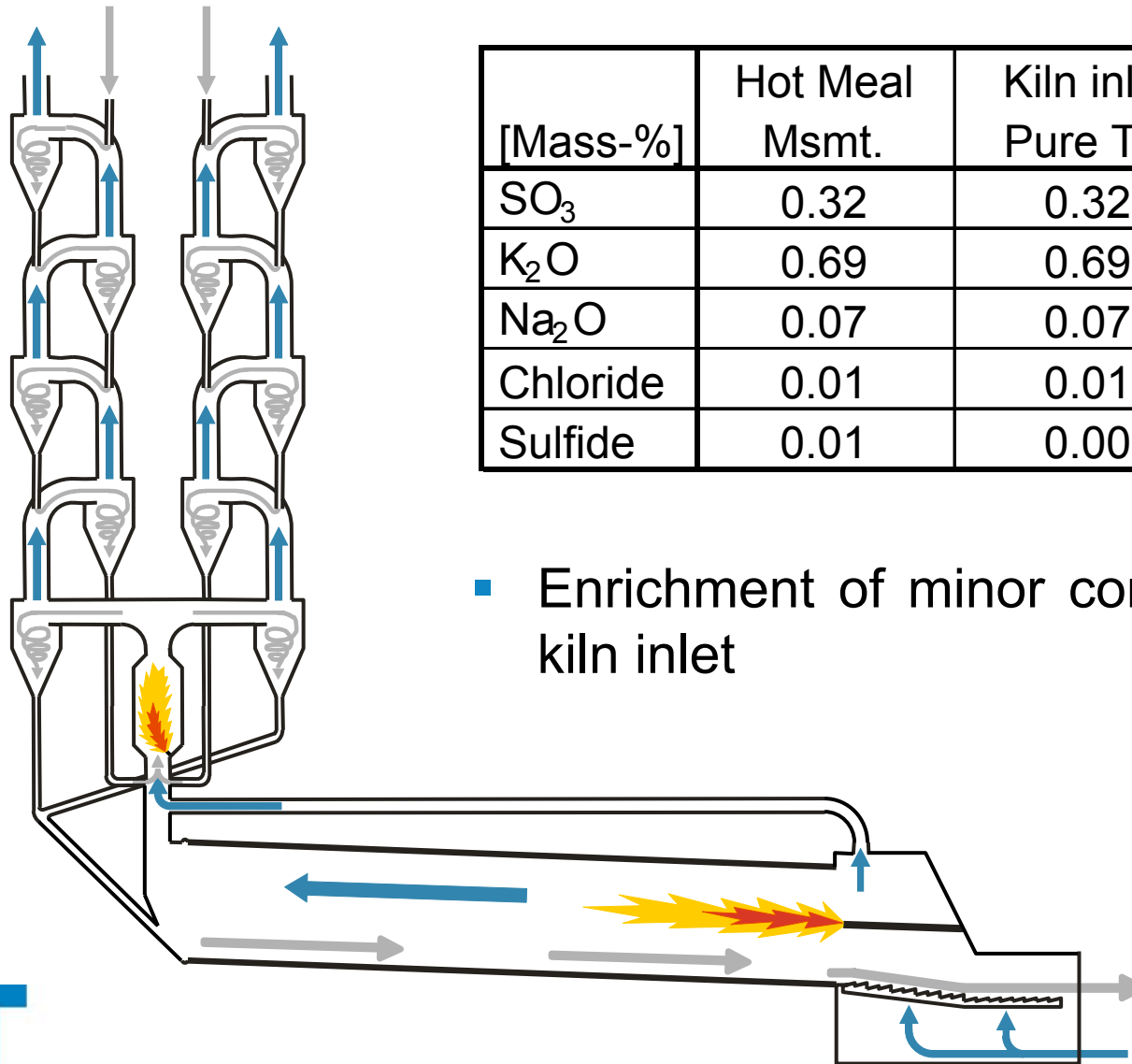
Introduction

- Computational thermochemistry is a strong tool to simulate the behaviour of complex chemical Systems
 - Restricted in pure form to ideal conditions
 - homogeneous mixing
 - no reaction kinetic inhibitions
 - However, many technical processes involve both, complex chemistry and incomplete mixing or kinetic inhibitions
- ⇒ Improve pure thermochemical model by process analysis and choice of a proper model structure

Cement production plant



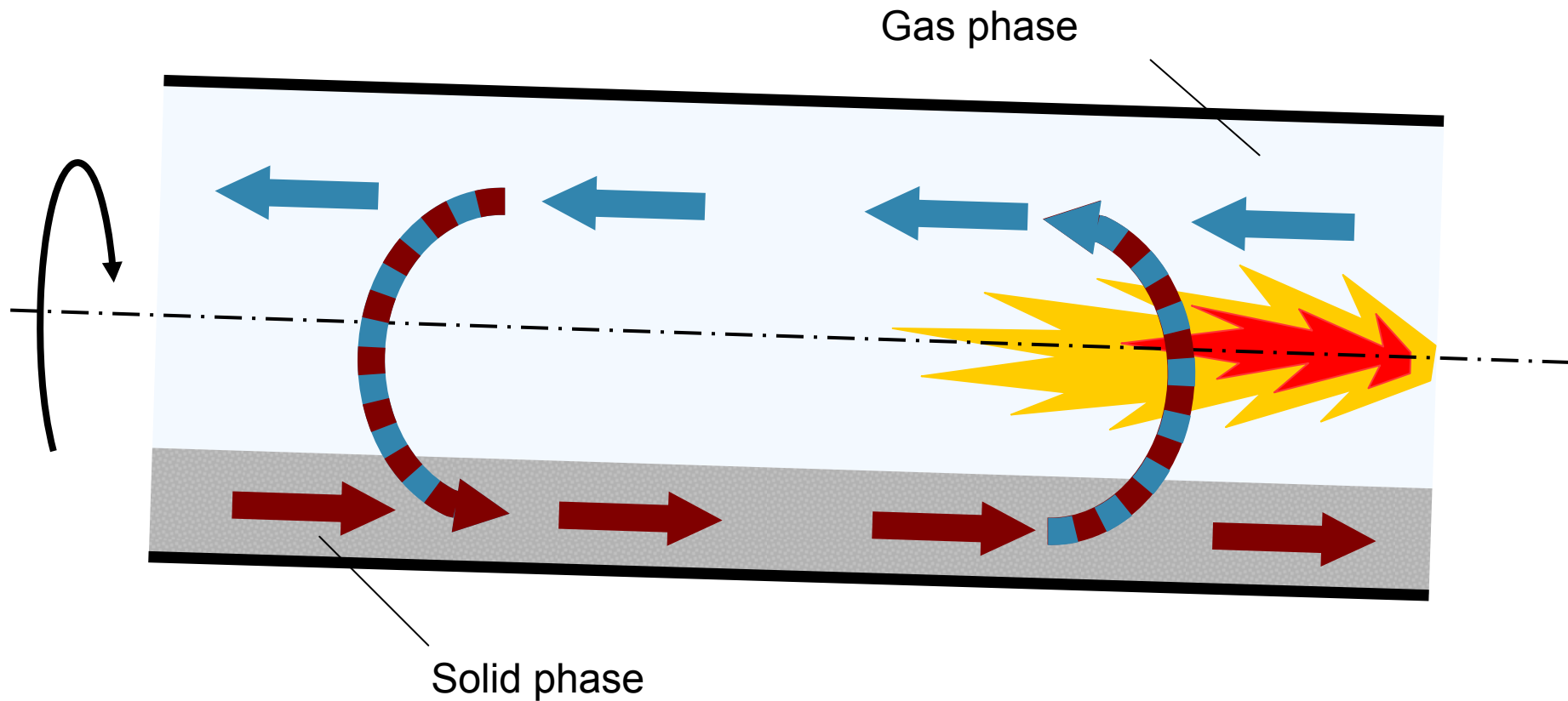
Minor components – Pure TC



[Mass-%]	Hot Meal Msmt.	Kiln inlet Pure TC	Kiln Inlet Msmt.
SO ₃	0.32	0.32	1.19
K ₂ O	0.69	0.69	5.20
Na ₂ O	0.07	0.07	0.11
Chloride	0.01	0.01	3.56
Sulfide	0.01	0.00	0.01

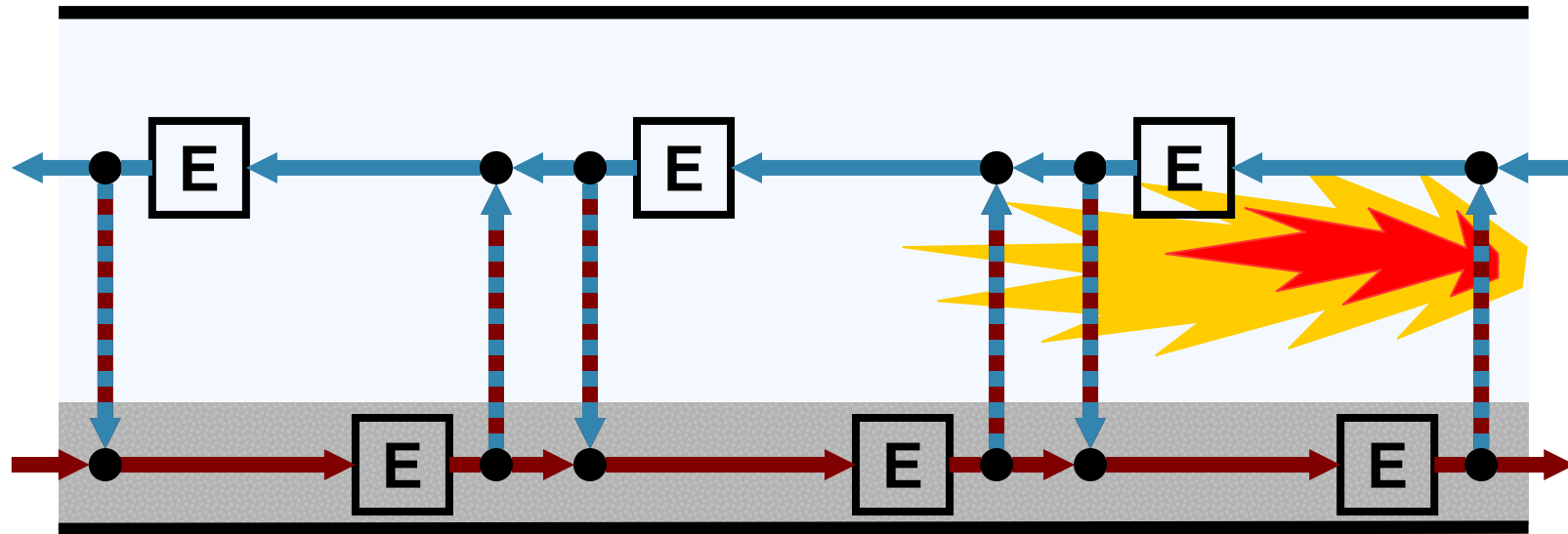
- Enrichment of minor components at kiln inlet

Transport conditions within a rotary kiln



- Mass exchange by
 - Rising and depositing dust
 - Vaporizing and precipitating volatile components

Process model

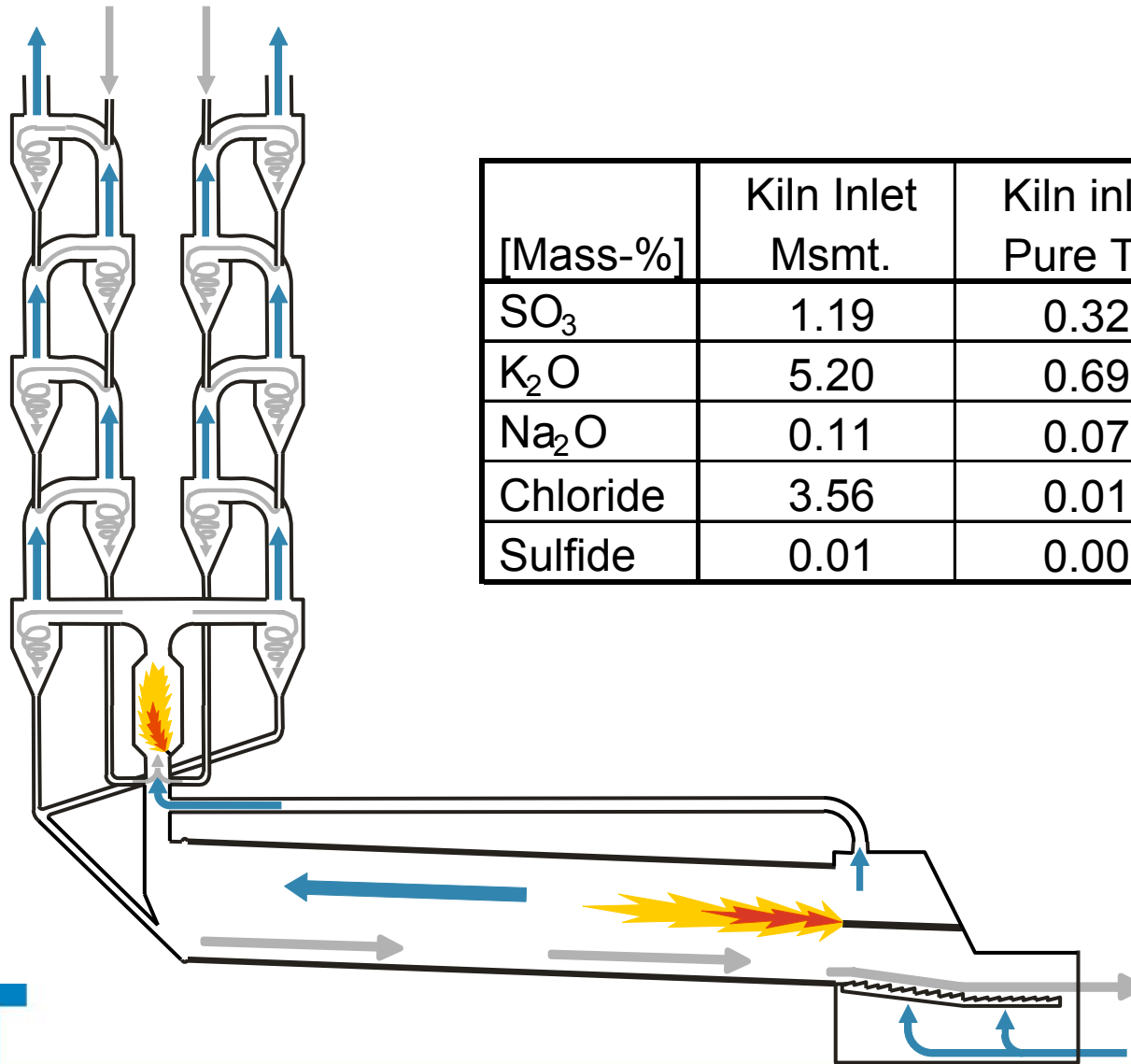


- Dust loading of gas phase
- Gas in between solid particles
(Frisch, 1983 / Brauers, 1971)

$$y_S = 0,2 \text{ kg Dust / kg Gas}$$

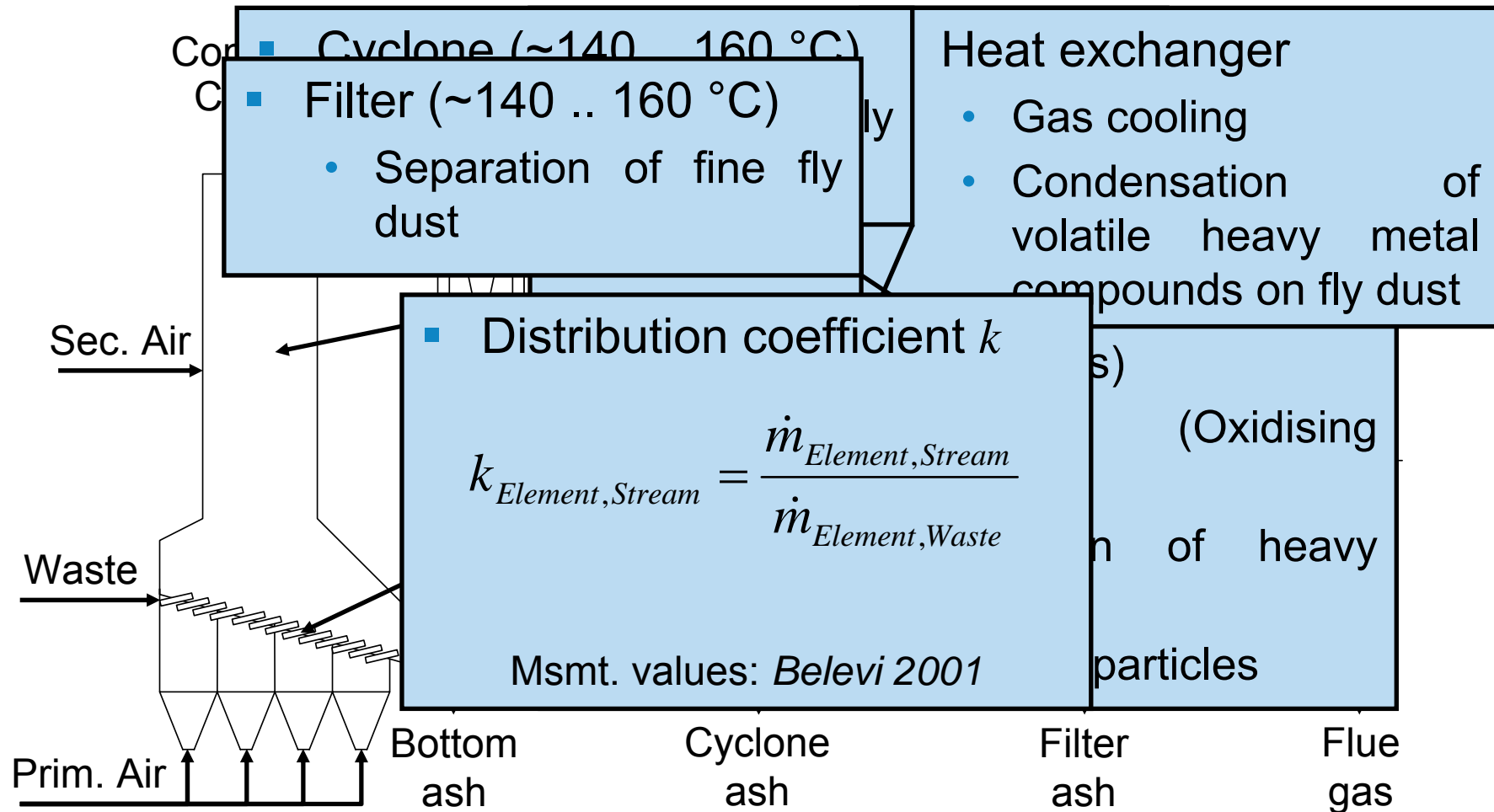
$$y_G = 10^{-4} \text{ kg Gas / kg Solid}$$

Results – Minor components at kiln inlet



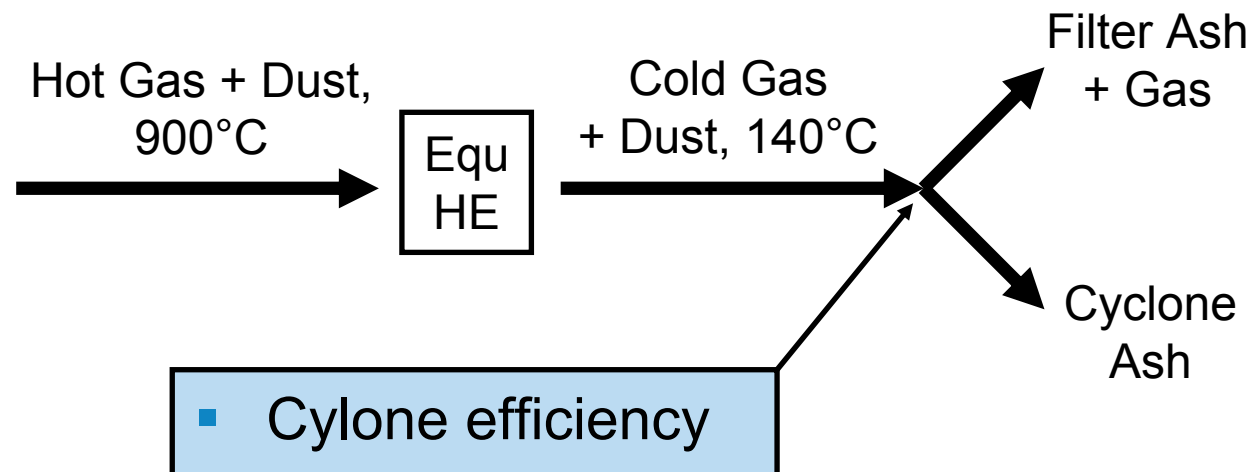
[Mass-%]	Kiln Inlet Msmt.	Kiln inlet Pure TC	Kiln inlet TC-Model
SO ₃	1.19	0.32	1.40
K ₂ O	5.20	0.69	1.87
Na ₂ O	0.11	0.07	0.10
Chloride	3.56	0.01	0.92
Sulfide	0.01	0.00	0.00

Waste incineration plant

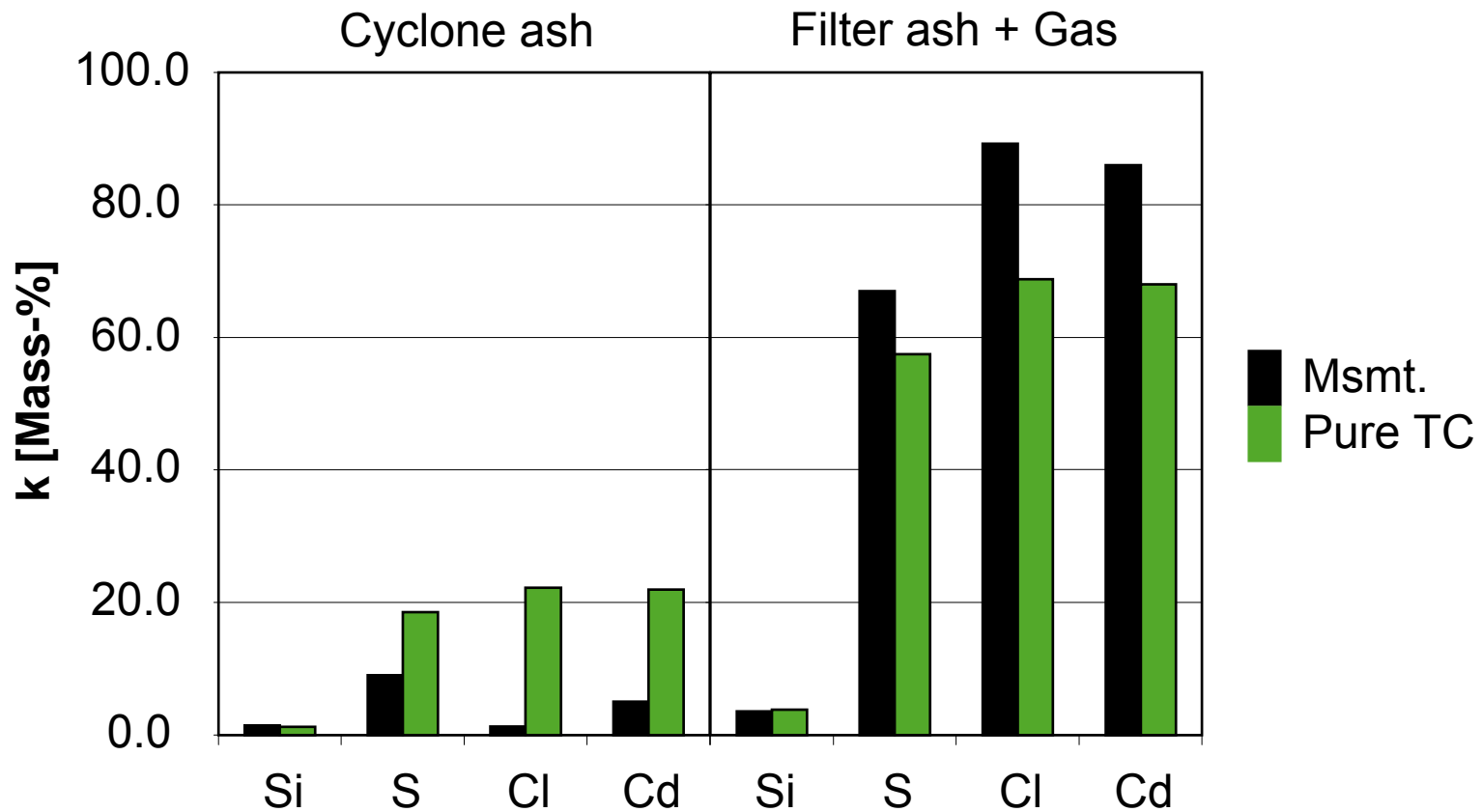


Fly ash composition – Pure TC

- Condensation of volatile heavy metals in the heat exchanger section



Fly ash composition – Pure TC



- Combustion chamber temperature: 900 °C

Heavy metal condensation on fly ash

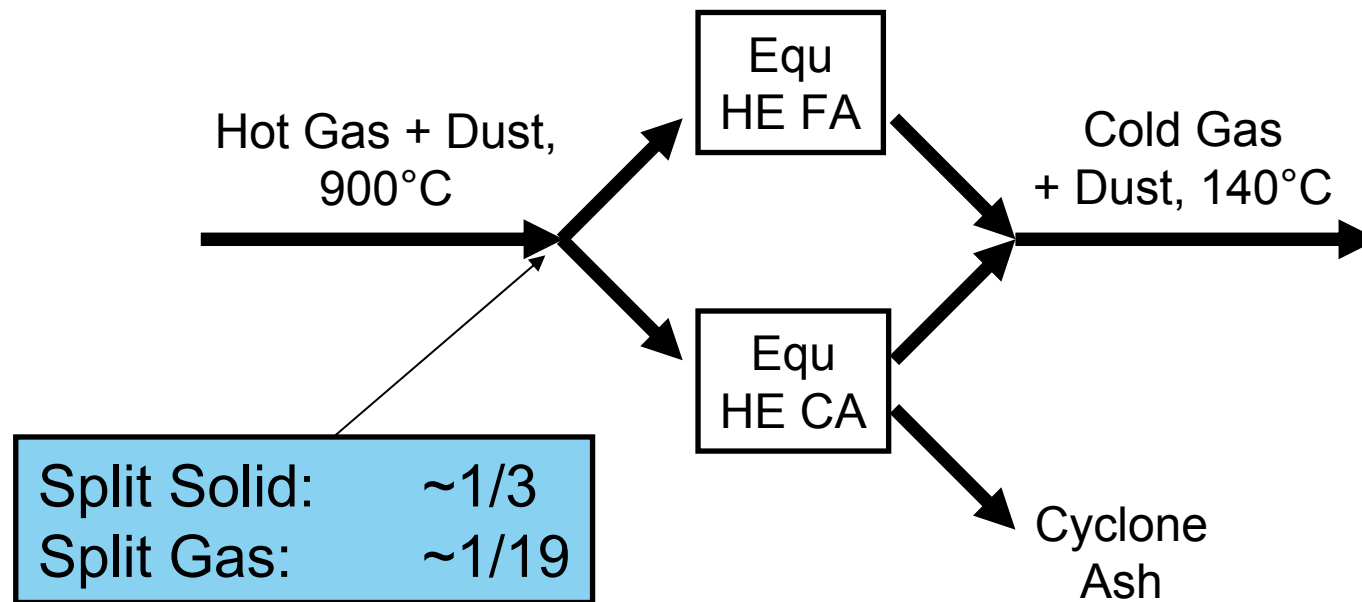
- Gaseous heavy metals condense on the surface of fly dust particles

- $$\frac{\dot{m}_{Cyclone\ ash}}{\dot{m}_{Filter\ ash}} \approx \frac{25\%}{75\%} = \frac{1}{3}$$

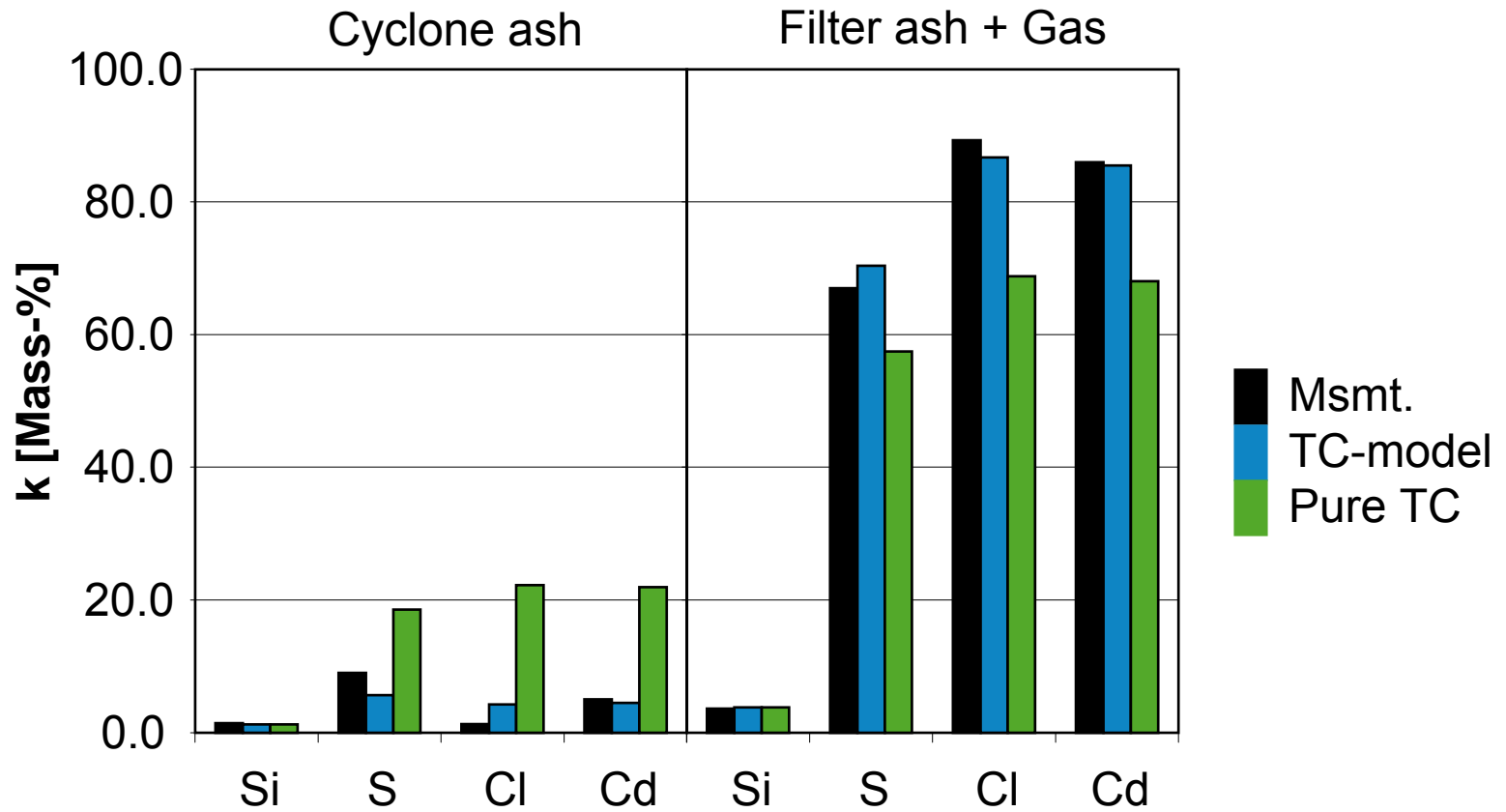
- $$\frac{S_{Cyclone\ ash}}{S_{Filter\ ash}} \approx \frac{5\%}{95\%} = \frac{1}{19}$$

- Separation of heavy metal compounds
 - Solid: By **mass** (~ 1/3)
 - Gaseous: By **specific surface area** (~ 1/19)

Heavy metal condensation on fly ash

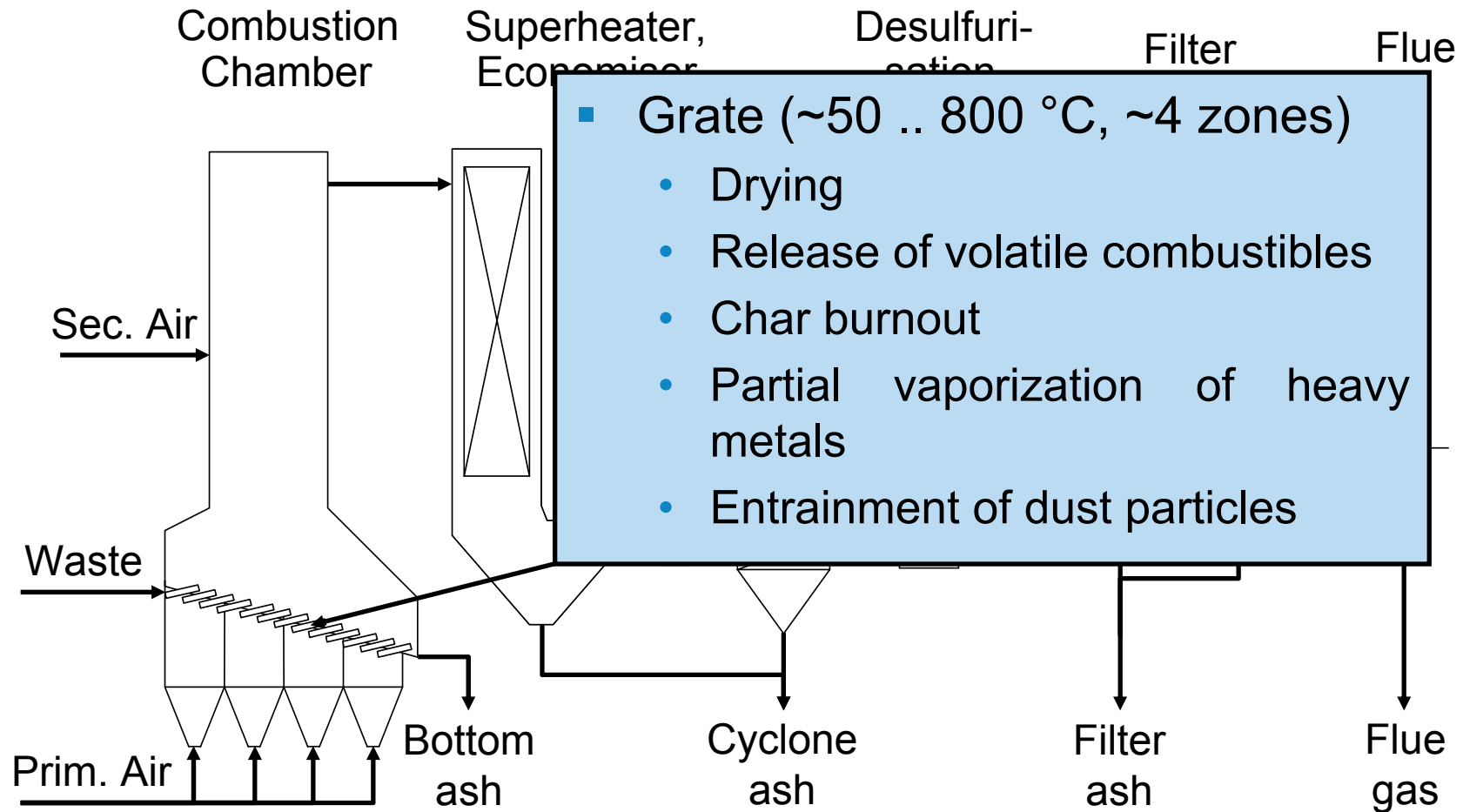


Results - Heavy metal condensation

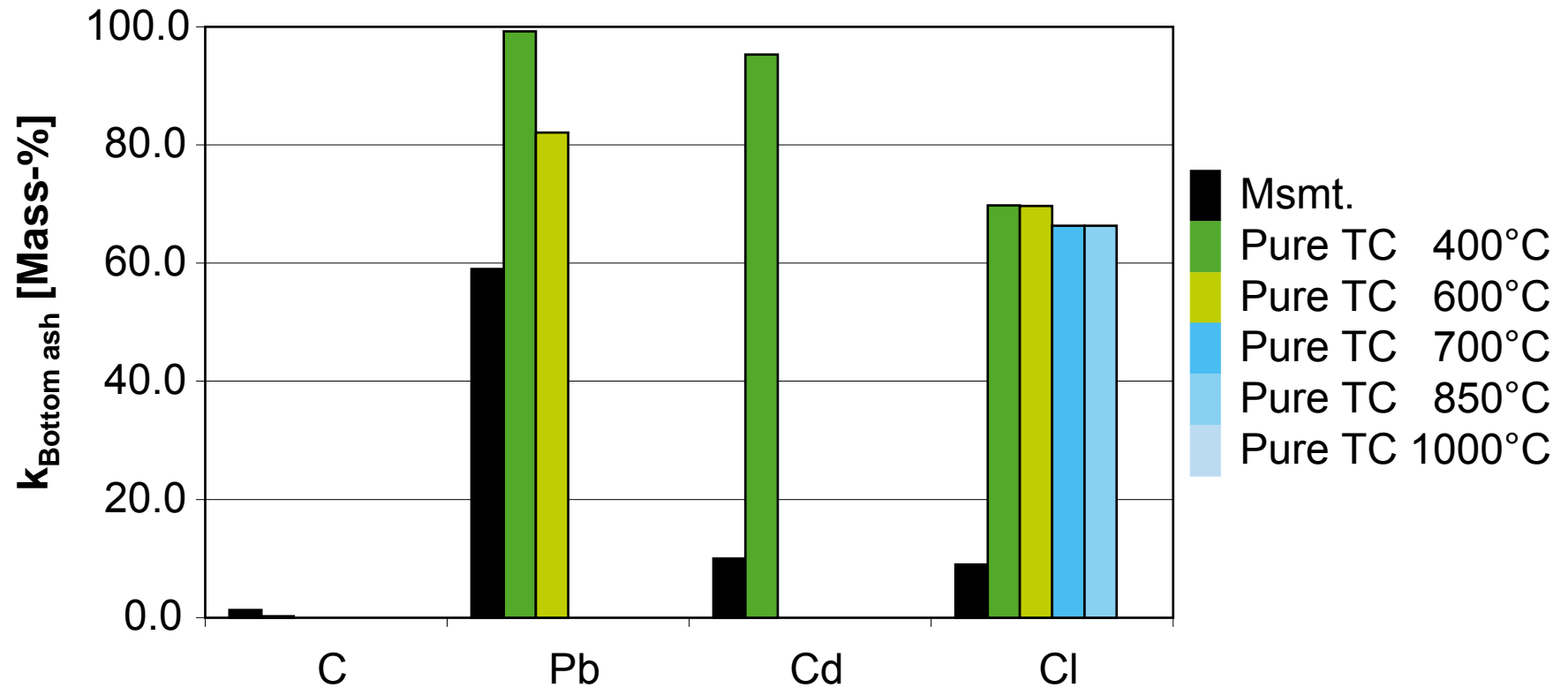


Mean Errors		Split gas phase	1/19
Pure TC	14.9 Mass-%	Split solid phases	1/3
TC-Model	6.5 Mass-%	T comb. chamb.	900°C

Grate Combustion



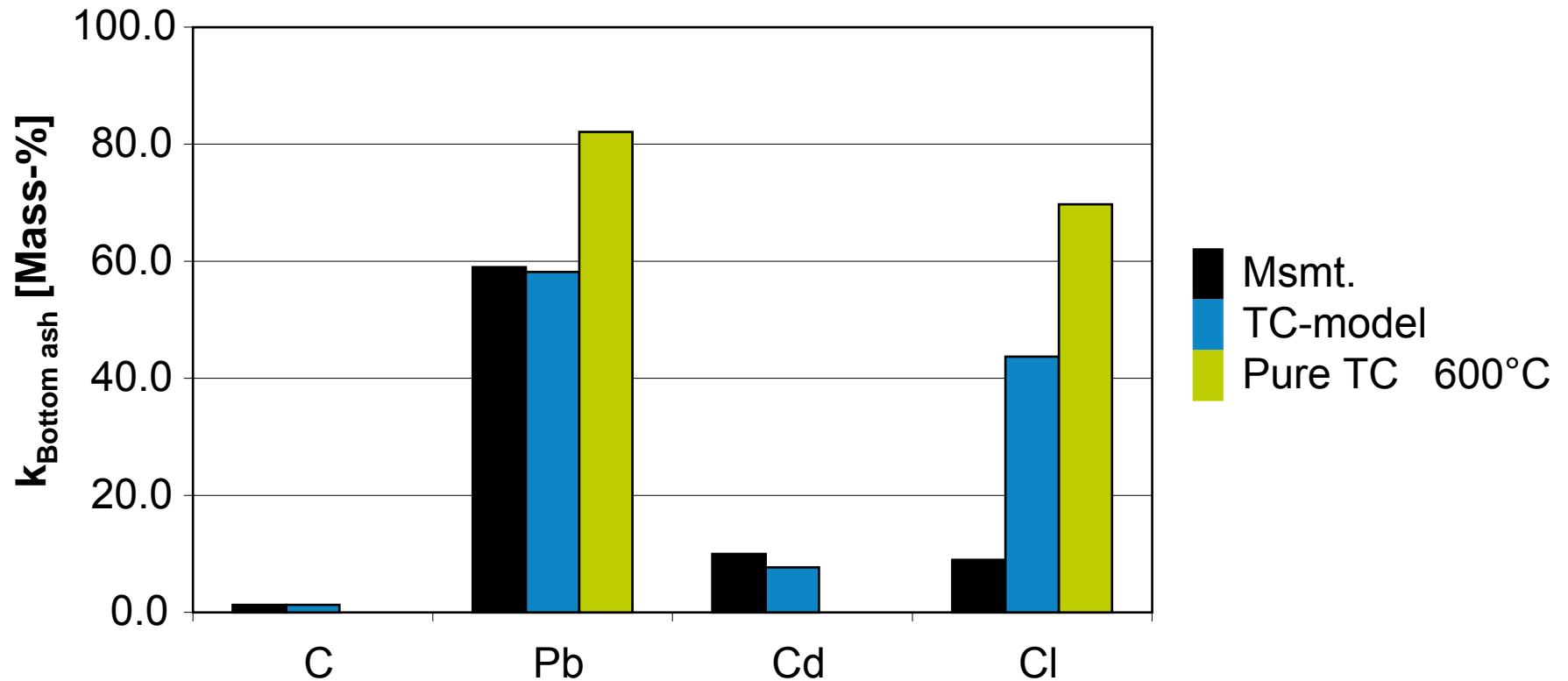
Grate Combustion – Pure TC



Grate Combustion – Qualitative Analysis

- Processes on the grate
 - Several distinct zones on the grate with separate air supply
 - ⇒ Varying temperature and oxidation conditions
 - Particles are entrained into the gas phase
 - ⇒ Fly Dust
 - Incomplete carbon burnout on the grate
 - ⇒ Residual C in bottom ash
- Modeling
 - Four equilibrium zones on the grate, different temperatures and air flow rates
 - Partial transfer of solids into the gas phase
 - ⇒ Correctly determine fly dust flow rate
 - Solid bypass around grate equilibrium zones
 - ⇒ Correctly determine residual carbon in bottom ash

Results - Grate Combustion



Mean Errors			
Pure TC	30.9 Mass-%	T Degassing Zone	620°C
TC-Model	22.2 Mass-%	T Burnout Zone	580°C

Conclusion and Outlook

- Computational thermochemistry is a strong tool to simulate the ideal behaviour of complex chemical systems
- Process analysis allows for incorporation of non-idealities by means of a properly chosen model structure and few simple and plausible assumptions
- ⇒ Significant improvement of modeling results
- Further improvement is possible but requires disproportionately more information
 - e.g. in grate combustion Cl is much easier released from PVC than from NaCl or KCl

AVT

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Thank you
for your attention!

RWTH