



A thermo chemical model of a reforming process using hydrocarbon fuels which is included in a fuel cell system

*Sven Wenzel
Oel Wärme Institut gGmbH, Aachen*



Contents

- Application Area of the CPO-SOFC-System
- Diagram of Process
- Equilibrium calculation based on ChemSheet
- Operation area of CPO-Process
- Influence of Anode-Offgas-Recirculation
- Conclusion

Application Area of the CPO-SOFC-System



stationary fuelcell block heat and power plant

- in areas with poor infrastructure
- supply of electrical power and heat

auxiliary power unit (APU)

- generates power independent from the engine (no idle-mode)
- air conditioning while the trucks are standing

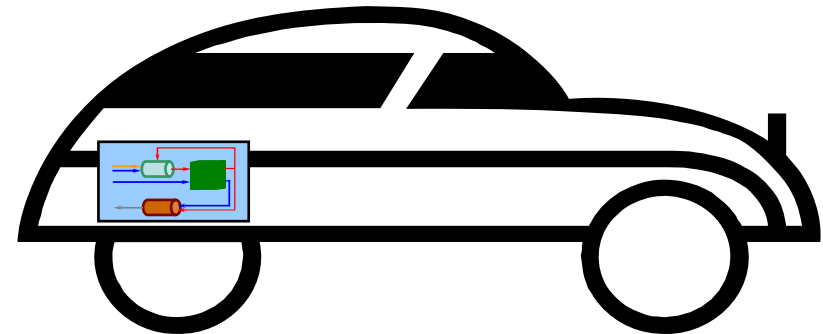
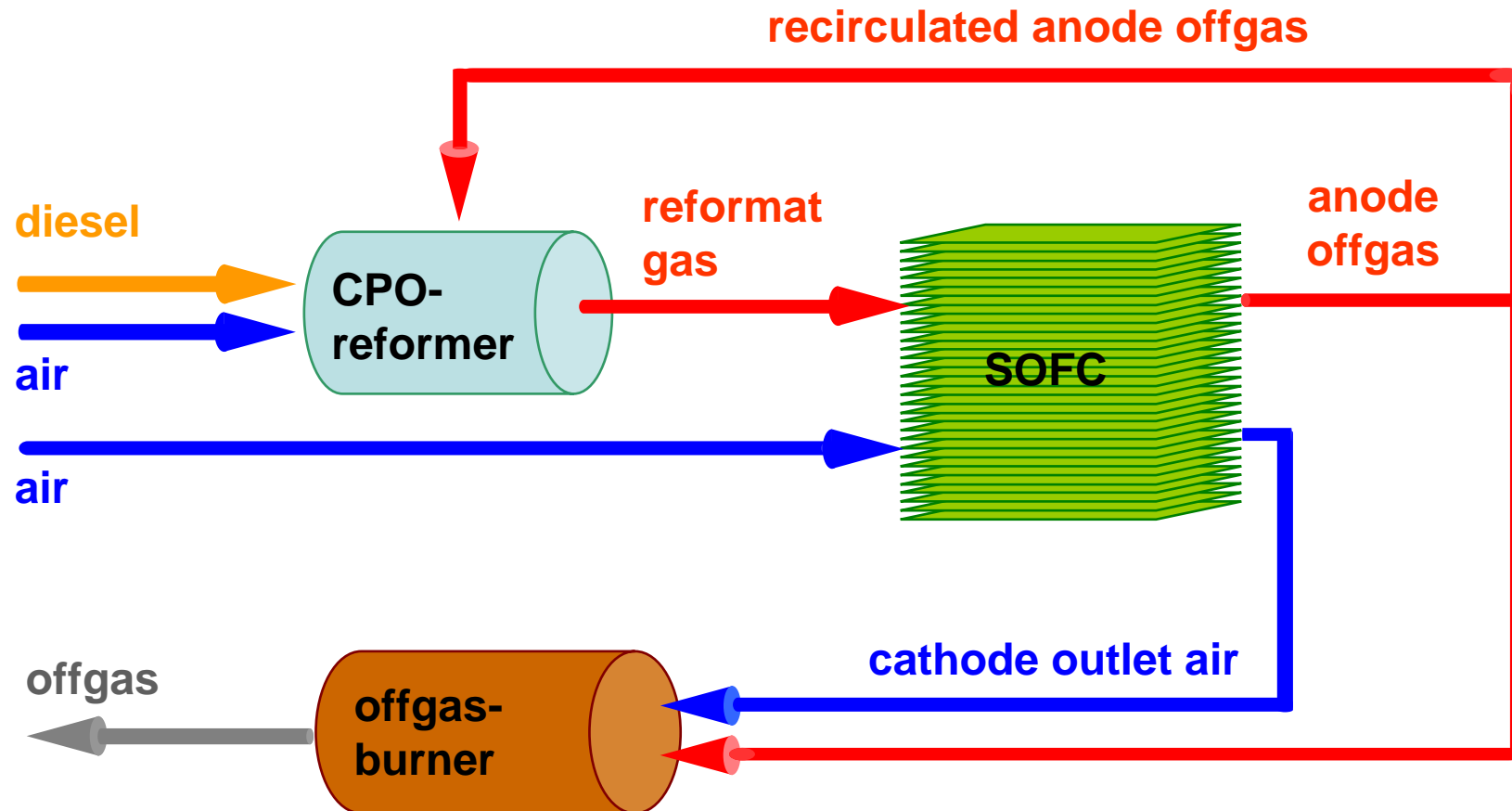


Diagram of Process



Excel Sheet – Input Stream Fuel and Air

Prozeßbild CPO - SOFC - Anodengasbrenner
Bei Änderung des Brennstoffs muß dieser noch manuell in ChemSheet geändert werden. Das Luftverhältnis bezieht sich auf C₂H₄. Brennstoffleistung wird automatisch bestimmt

pressure | **fuel** | **air ratio**
initial value

temperature | **air ratio**
step size

power | **number**
of steps

heat flow

reaction
temperature

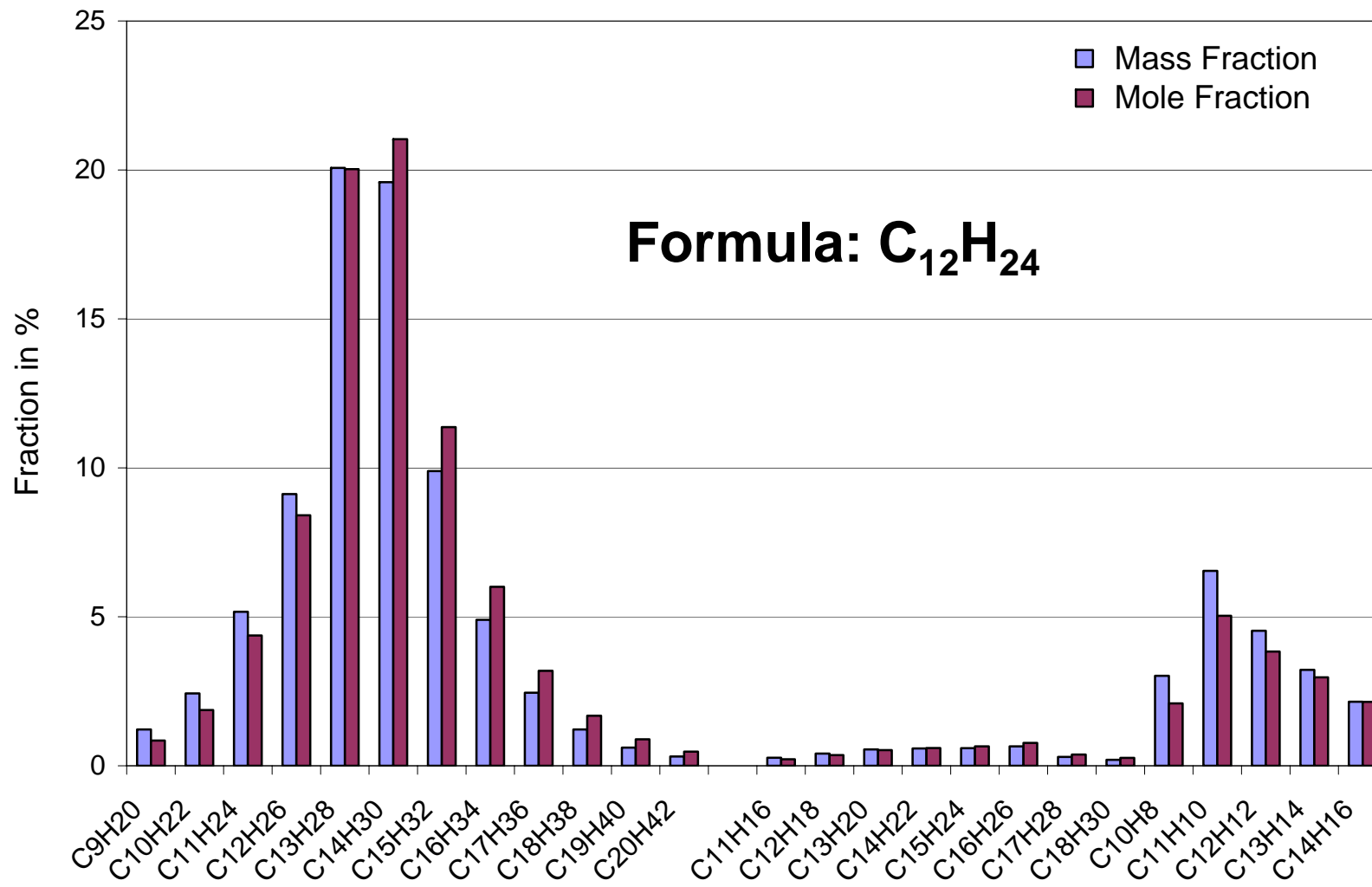
Eingangsstrome		Mischtemperatur	h-CPO	
Temperatur [°C]	Druck [bar]	261,05 °C	Startwert	0,4
25	1		Laufintervall	0,38
Leistung [kW]	5		Anzahl Lambdaschritte	2
Edukte	Stoffmenge [mol/s]		Endwert Lambda:	0,39
C 12,95			CPO	
H 24,38	0,000642			
Enthalpiestrom [J/s]	-220,30		Step	1
			Stepnumber	5
			Conditions	
			Wärmestrom [J/s]	0,00
			Wärmestrom [kW]	0
			Wärmestrom [%]	0,00
			Druck [bar]	1
			Results	
			EnthalpieDiff [J/s]	0,00
			Temperatur [°C]	921,39
			Enthalpie [J/s]	-27120,27
			Enthalpiestrom [J/s]	-1248,43
			Wirkungsgrad [%]	85,43
			Übertragungsverluste [%]	0,00
			Bed. Stöck Rez.	0,013

Luft		Stoffmenge
Temperatur [°C]	Druck [bar]	
20	1	
Luft	Stoffmenge [mol/s]	
O ₂	0,00489	
N ₂	0,0184	
Summe	0,02328	
Enthalpiestrom [J/s]	-3,40	
Feuchtigkeit		
Temperatur [°C]	20	
Relative Feuchte [%]	0	
Masse Dampf [kg]	0	
Wasser [mol/s]	0	

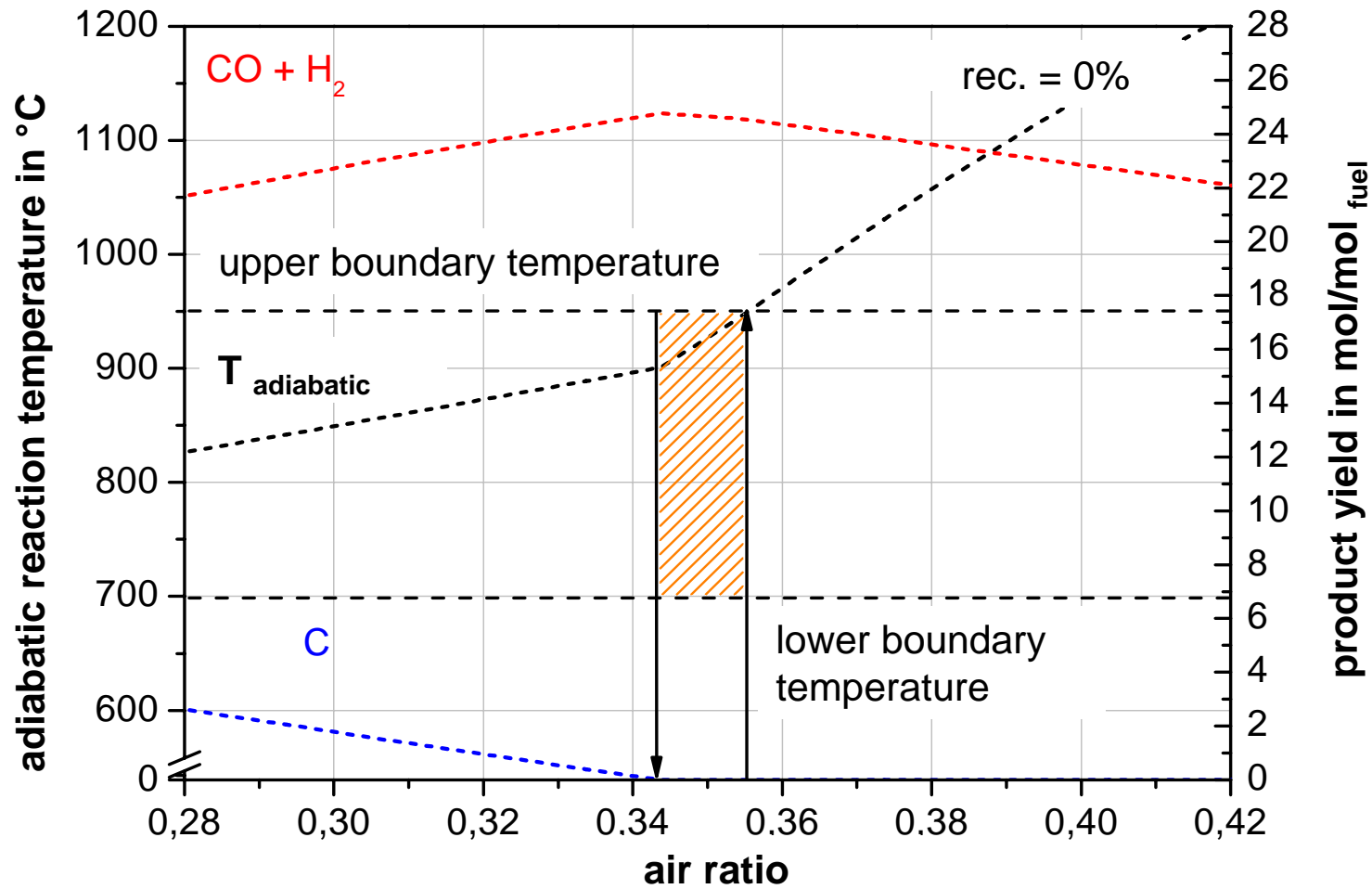
Excel Sheet – Products Reformat

	Ausgabe		
	Eingabe bedingt (über Drop-Down)		
	Eingabe		
quantity of materials	Produkte	Stoffmenge [mol/s]	Bedingung
	CPO		
	H2	7,603E-03	entered
	H2O	2,828E-03	entered
	CO	8,698E-03	entered
	CO2	2,385E-03	entered
	CH4	2,943E-07	entered
	C2H2	1,535E-13	entered
	C	0,000E+00	abgelagert
	N2	2,452E-02	entered
	O2	8,1021E-19	entered
	NO	6,4906E-14	entered
	CxHy	0,0000E+00	entered
	Summe	0,0460	
			Aktivität
			6,394E-06
			0,0140957
			activity

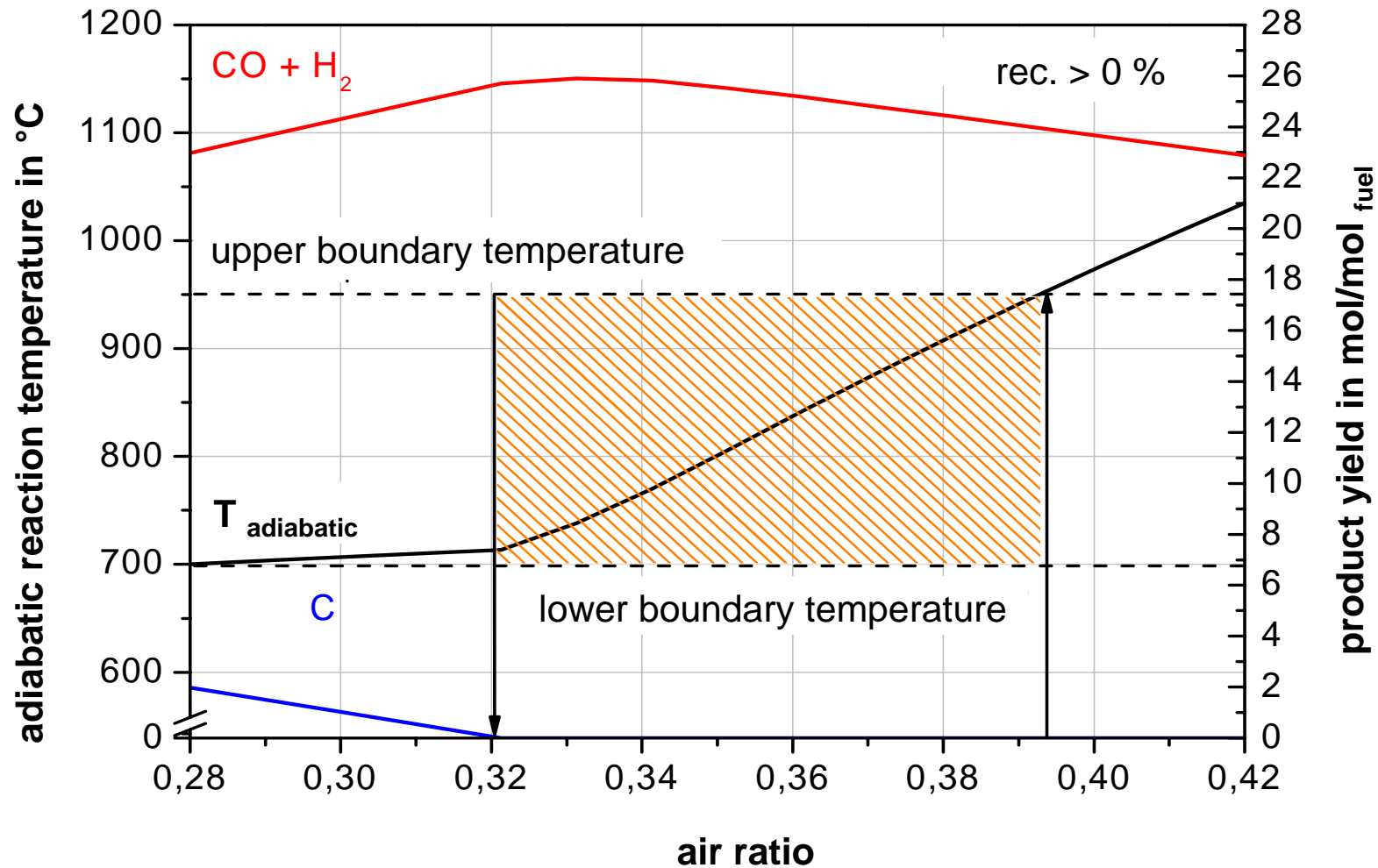
Model Fuel (according to Amphlett) for Material Data Bank



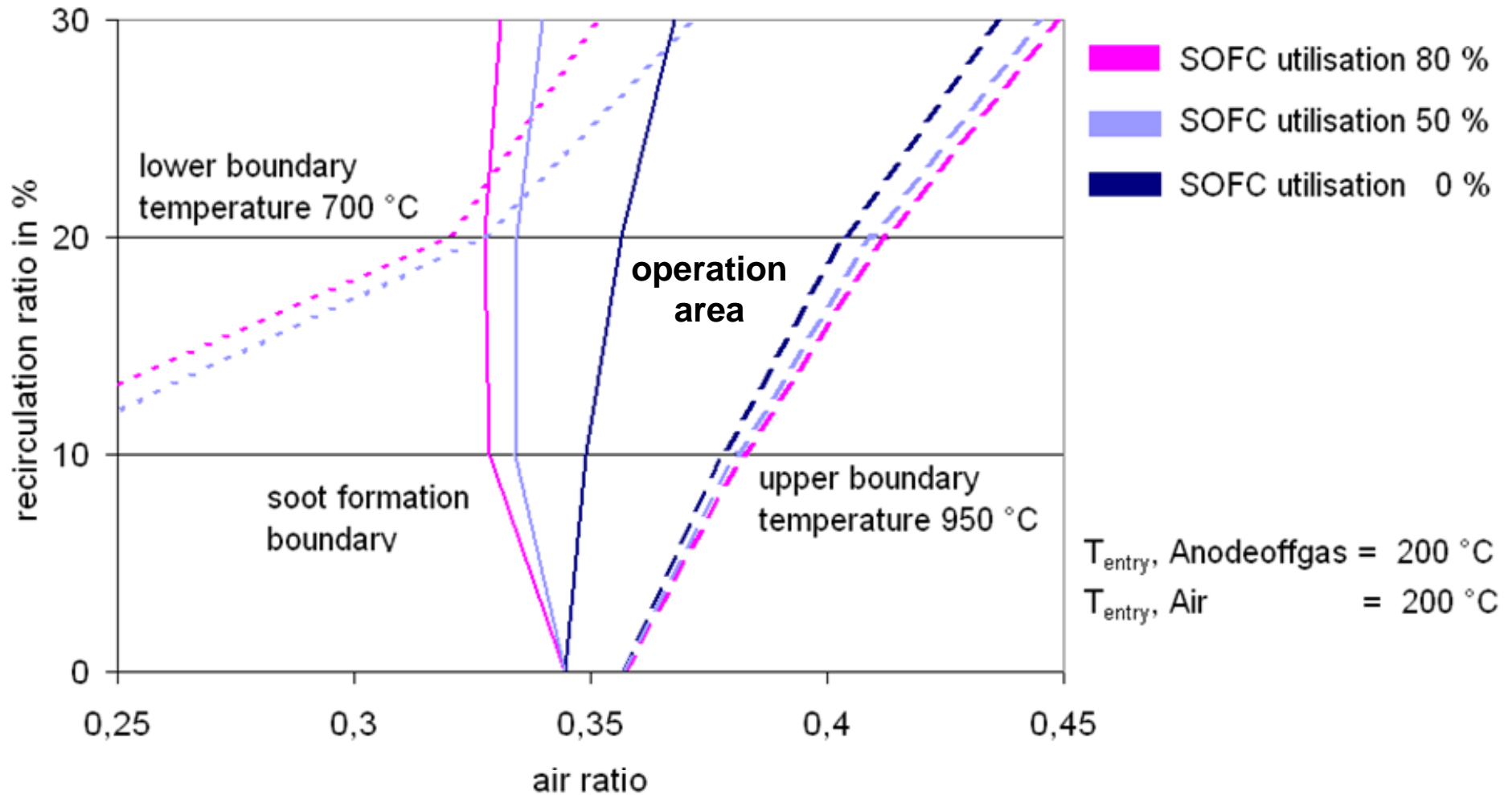
Operation Area of CPO-Process



Operation Area of CPO-Process with Anode-Offgas Recirculation



Operation Area Depending on Recirculation Ratio and SOFC-Utilisation



Conclusion

- catalytic partial oxidation is possible for stationary and mobile applications
- restricted operation area of CPO-process between soot-formation and boundary temperature of catalyst
- the equilibrium calculation based on ChemSheet shows the potential of recirculation of anode-offgas
- increase in the part of recirculated anode-offgas enlarges the operation area of CPO-process